

# Troubleshooting Paper Machine Water Systems with a Portable Flowmeter

Jeff Fochs

[jfochs@cleantechpartners.org](mailto:jfochs@cleantechpartners.org)

715.571.9385





# **“If you don’t measure it, you can’t manage it.”**

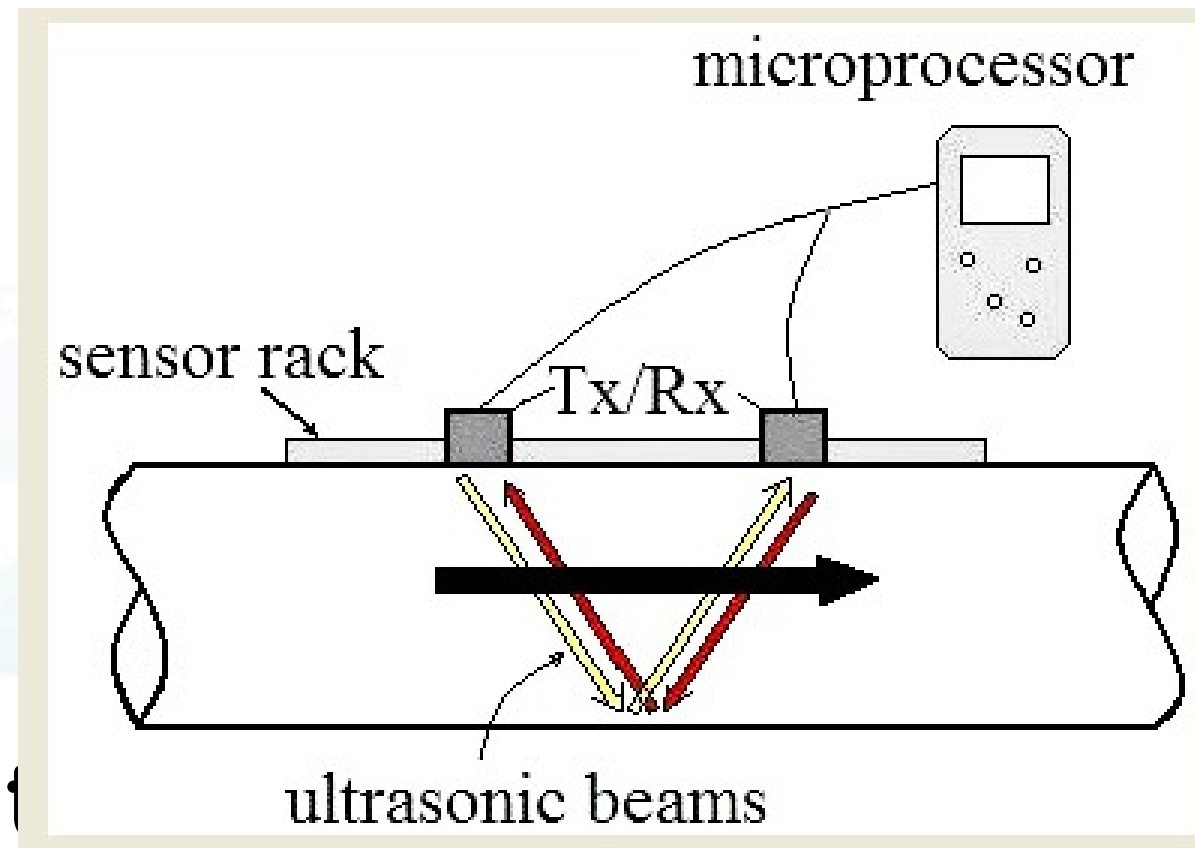
**In a mill setting, it is not practical to have permanent flow meters on everything. Some facilities have more complete instrumentation than others, but it is not reasonable to instrument everything.**

- Utilize portable, ultrasonic flow measurement**
- Transit time**
- Doppler**

# Ultrasonic Transit Time Flow Meter



# Ultrasonic Transit Time Flow Meter Configuration



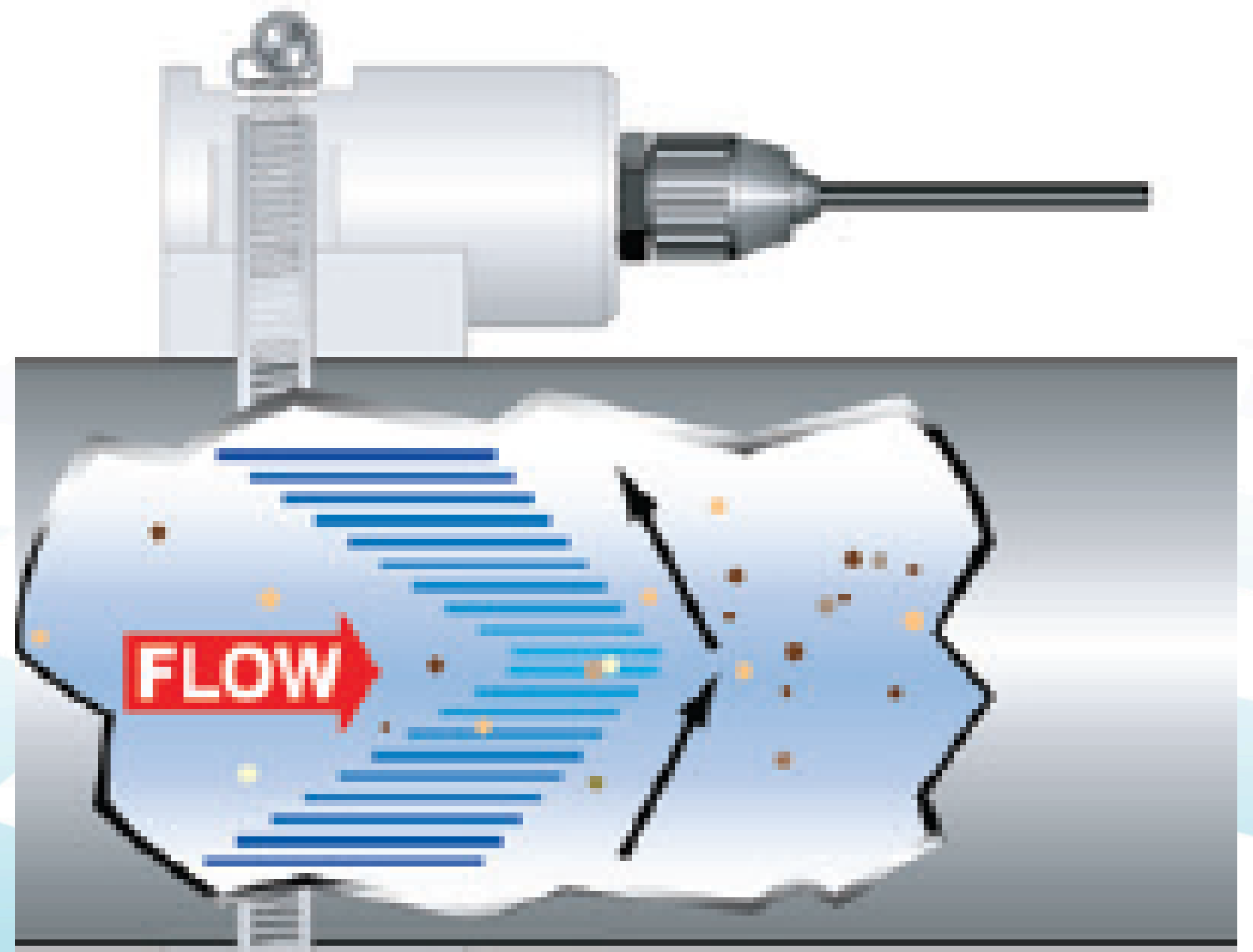
- Measures time it takes to travel upstream and downstream
- Calculates flow based on difference

# Ultrasonic Transit Time Flow Meter

- Works well on water and other fluids
- Works on steel, stainless steel, copper, plastic, but not galvanized pipe
- Maximum temperature 375 degrees F. (GE Panametrics PT-878)
- Sound speed of pipe material and fluid must be known (or determined)
- May need to experimentally determine sound speed for unknown fluids
- Pipe must be full
- Recommended setup parameters are not unlike most flow meters (10 pipe diameters of straight pipe upstream and 5 downstream)
- Vibration may cause unstable operation
- Vapor bubbles may interfere with operation
- Does not work with high levels of suspended solids (typically > 1%)

# Ultrasonic Doppler Flow Meter

**Measures speed of  
particles or bubbles in  
fluid**



# Ultrasonic Doppler Flow Meter

- Does not require material sound speed information
- Requires particles or bubbles in fluid for operation
- Does not work with clear fluid
- May give erroneous readings if pipe is not full
- Velocity in pipe must be high enough that particles do not settle

# Flow Measurement Surprises

- Paper machine dryer drainage condensers
- Paper machine warm water tank balance
- Paper machine showers (worn shower nozzles can double water consumption)
- Vacuum pump seal water management
- Rotating equipment seal or packing water (seals controlled with ball valve average 2.7 gpm)
- Fill valves (manual or controlled) on whitewater tanks, pulpers, etc. that appear to be shut
- Flows to heat exchangers (need to be in recommended range for good performance)
- Evaporator surface condensers

# Dryer Drainage Condenser Troubleshooting

Condenser cooling water control valve is wide open, but not achieving desired vacuum.

## How is vacuum created?

At a vacuum of 15" Hg, steam takes up ~3,200 times the volume of an equivalent mass of water. Collapsing steam to water creates a void, which in turn establishes vacuum. **Turning steam into water is the job of the condenser.**

Air is present in steam. In order to maintain vacuum, it must be removed from the condenser. **Removing air is the job of the vacuum pump** (or other air removal system).



# Dryer Drainage Condenser Troubleshooting



# Dryer Drainage Condenser Troubleshooting

The first step is to determine whether the condenser or air removal is limiting vacuum

- Measure temperature at condensate pump.
- Check condensate receiver vacuum
- Consult steam tables to determine if condensate is at saturation temperature

Inches Hg vacuum	Pressure PSIA	Pressure PSIG	Temperature °F		Inches Hg vacuum	Pressure PSIA	Pressure PSIG	Temperature °F
28	0.9	-13.8	99.7		12	8.8	-5.9	187.2
26	1.9	-12.8	124.6		10	9.8	-4.9	192.1
24	2.9	-11.8	140.3		8	10.8	-3.9	196.7
22	3.9	-10.8	151.7		6	11.8	-2.9	200.9
20	4.9	-9.8	161		4	12.7	-2	204.8
18	5.9	-8.8	168.9		2	13.7	-1	208.5
16	6.8	-7.9	175.8		0	14.7	0	212
14	7.8	-6.9	181.8					

# Dryer Drainage Condenser Troubleshooting

**If condensate is subcooled, vacuum is being limited by air removal system**

- **Vacuum pump may not have adequate seal water flow**
- **Vacuum pump may be in poor condition**
- **There may be excessive air leaking into system**
- **Air removal system may not be capable of providing desired vacuum (specific air volume gets larger with greater vacuum)**

# Dryer Drainage Condenser Troubleshooting

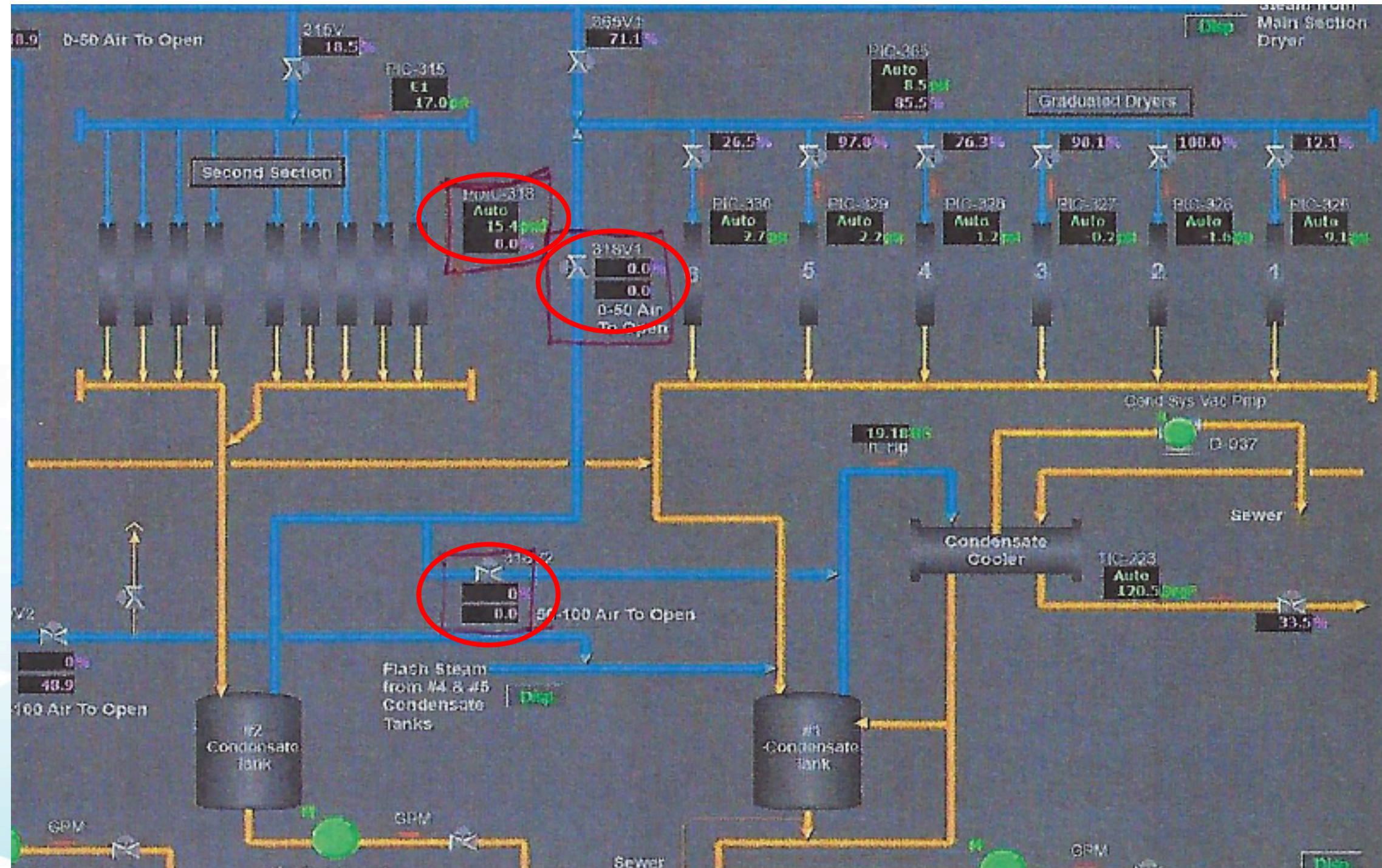
**If condensate is at saturation temperature, vacuum is being limited by the action of condenser**

- **Condenser fouled**
- **Water flow inadequate**
- **The amount of steam reaching condenser may be greater than design flow (overloaded condenser)**

# Dryer Drainage Condenser Overloaded

- **Weak or inappropriately designed thermocompressor**
- **Incorrect or damaged syphons**
- **Excessive dryer differential pressure**
- **Improper cascade pressures**
- **Vent valve(s) open or leaking through when shut**

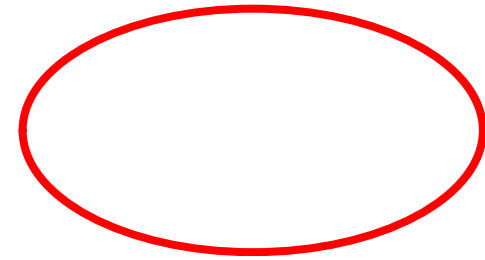
# 3<sup>rd</sup> Section Differential Pressure Out of Control



Both 3<sup>rd</sup> section differential pressure control valves are shut, but differential is much greater than set point – vent valve leaking



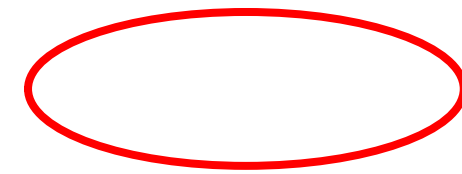
# Hot Water Tank Out of Balance



There is leaking through 152 gpm, while recirculating pump is sending 370 gpm to



# Hot Water Tank Out of Balance



# Pumps Operating in Parallel



**Two (or more) pumps operating in parallel.  
Are they all doing their fair share?**

# Pumps Operating in Parallel

Plant operating (2) centrifugal pumps in parallel to provide raw water. Both pumps were designed for the same duty (10,000 gpm @ 92' head). One pump was an older, non-current model and the other was almost new.

- Portable flow measurements indicated the new pump was providing 5,200 gpm @ 112' head (correlated well with published curve)
- The old pump was not pumping at all!
- The old pump was using more electricity than the new one (265 vs. 255 hp)
- Casing on the old pump was 50 degrees warmer than raw water
- Pumps had been operating in this mode for several months
- Recommended replacing pump with a more appropriate design. Existing pumps 30 to 50% efficient, recommended unit >80%.

# Pumps Operating in Parallel

- Operating below minimum flow can be harmful to pump (although the previous example did not seem to mind)
- Operating a pump below minimum flow can cause shaft breakage due to cavitation at the cutwater
- Multi-stage pumps are especially prone to failure due to low flow because heat can't get away
- Most multi-stage pumps have some type of recirculation device to keep them above minimum flow
- Parallel pumps must be carefully designed for expected conditions
- In some cases, a smaller pump for winter conditions and larger pump for summer may be appropriate
- Installing a variable speed drive can save energy but is not a substitute for appropriately sized pumps

# Excessive Seal Water Flow to Liquid Ring Vacuum Pumps

- Measured seal water flow to Nash CL2002 at 90 gpm (specification for applications up to 20" Hg is 20 gpm)
- Power usage with 90 gpm seal water flow was 104 hp.
- Slowly reduced seal water flow while also measuring power usage.
- Power usage continued to drop along with seal water flow.
- Ended up with 21.6 gpm seal water flow with power usage of 97 hp (reduction of ~7%)

# Liquid Ring Vacuum Pump Seal Water Heat Recovery

- Flow and temperature measurements taken at several mills reveal the heat equivalent of ~70% of vacuum pump horsepower ends up in seal water.
- For a paper machine using 4,000 hp to drive vacuum pumps, this is over 7 MMBtu/hr (7,000 pph steam).
- In most mills, seal water heat is either sent to the outfall or a cooling tower.
- For mills that heat water or stock, heat from vacuum pump seal water can reduce mill steam usage.
- **There are three primary methods by which vacuum pump heat can be utilized**
  1. By use of heat exchanger for fresh or whitewater heating
  2. Direct usage of whitewater as vacuum pump seal water
  3. Utilize heated fresh water from vacuum pumps for showers, etc.

# Heat Exchanger To Recover Heat From Seal Water

- Seal water delta T of 15 to 35 degrees F requires a large heat exchanger with low approach temperature to transfer useful heat.
- Plate and frame heat exchangers are lowest capital cost option but tend to foul quickly.
- Spiral heat exchangers have the highest capital cost but usually operate trouble free from an operations standpoint.
- Cascading seal water (first through high vacuum pumps, then pumps that operate at lower vacuum levels) can decrease total seal water flow and increase delta T which allows for better heat transfer and a smaller heat exchanger.

# Direct Use Of Machine Whitewater For Vacuum Pump Seal Water

- No need for a heat exchanger
- All heat is used beneficially
- Whitewater chemistry may not be compatible with vacuum pump metallurgy
- Particulates in whitewater may plug seal water orifice plates or build up in vacuum pumps
- Whitewater at high temperature may reduce vacuum pump performance

# Use Warm Vacuum Pump Seal Water For Showers

- Requires robust pre-separators to prevent contamination
- Machines that have an existing sump for vacuum pump seal water are good candidates
- Recommend turbidity monitor and/or separator high level interlocks
- Several mills have direct discharge permits for vacuum pump seal water (require reliable systems to ensure permit compliance)
- Very practical for mills that heat significant amounts of fresh water
- Warm water can also benefit rotating equipment (pumps, agitators, etc.) mechanical seals. Seal water infiltrating whitewater system will end up being heated to process temperature



# Use Vacuum Pump Seal Water For Showers





# Questions?

**Jeff Fochs**

**Cleantech Partners**

**[jfochs@cleantechpartners.org](mailto:jfochs@cleantechpartners.org)**

**[Jeff.fochs@focusonenergy.com](mailto:Jeff.fochs@focusonenergy.com)**

**715.571.9385**